

# Elizabethan source, 21<sup>st</sup> Century treatment

*Innovative Applications of Materials Chemistry in Water Treatment:  
Part 1 Removal of Contaminants from Drinking Water*

Chris Rockey  
May 16

# Acknowledge and explain...



# Contents

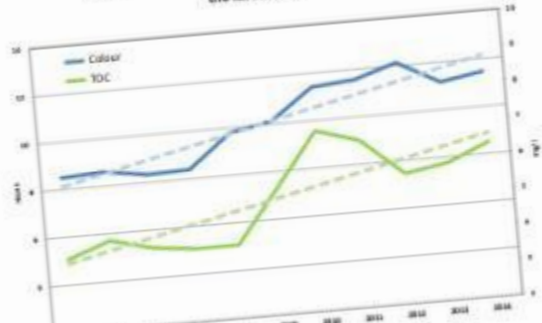
- Motive and opportunity
- Suspended ion exchange, in-line coagulation, ceramic microfiltration
- DOC, membrane fouling and DBPs
- Full scale application



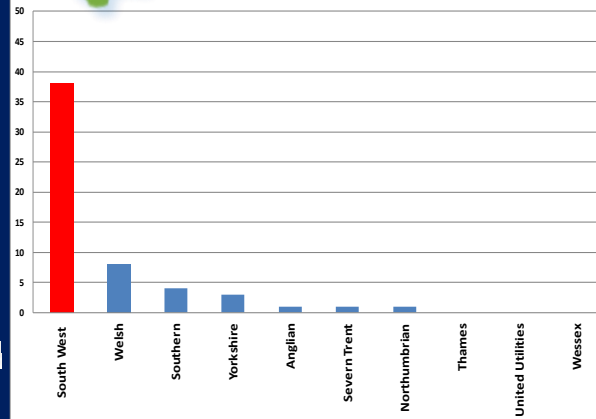
# Motive...



Increasing colour and TOC in raw water sources over the last decade



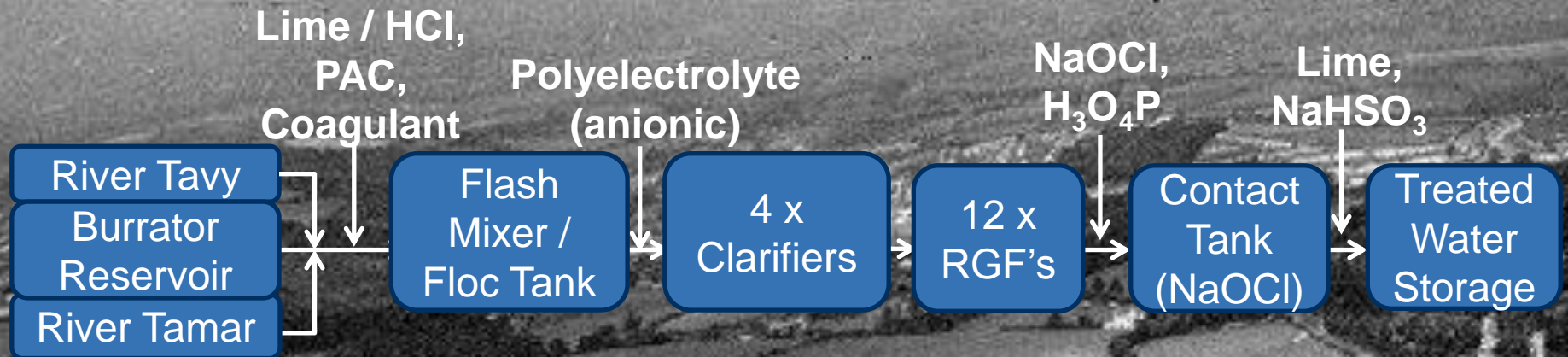
% Zones >50ug/l Total THM's




# Opportunity



# Rural Crownhill WTW c1955



# Constrained Crownhill c2016

- 
- The image is an aerial photograph of an industrial facility, likely a water treatment plant, outlined in red. The facility includes several large rectangular buildings, numerous circular tanks, and extensive parking areas. The surrounding area consists of residential housing and other commercial buildings. A blue callout box in the lower-left corner contains a list of issues.
- Access, neighbours and pumping
  - Contact tank, GAC and other improvements
  - Inappropriate use of space within the city

# Reviewed and re-stated treatment goals

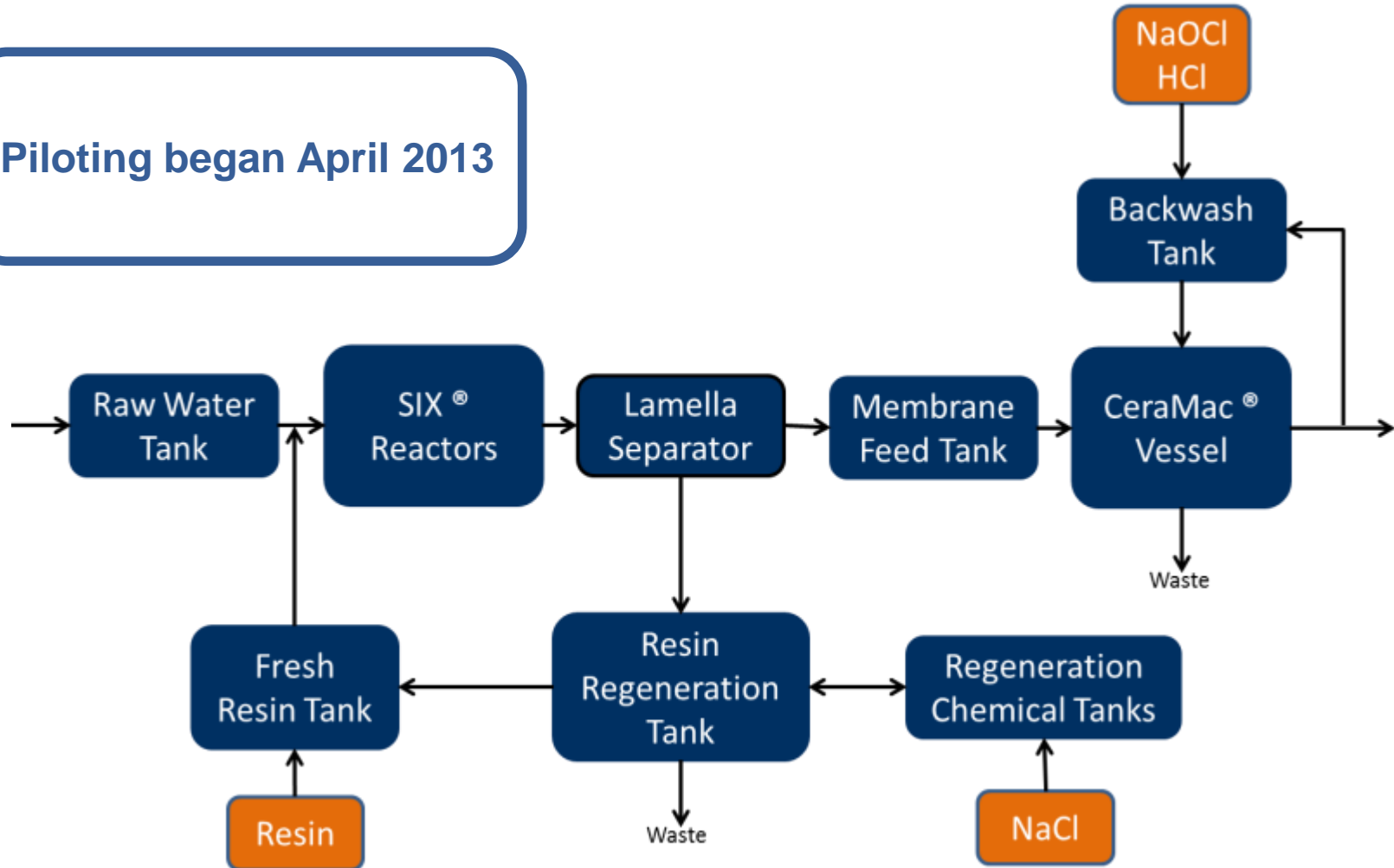
- **Absolute Barrier to Cryptosporidium**
- **DOC / disinfection by product reductions**
- **Very compact, forward looking design**
- **Highly automatable, robust and efficient process**
- **Environmental impact/sustainability**
- **Keep consumer bills down in long term**





# Pilot testing

Piloting began April 2013

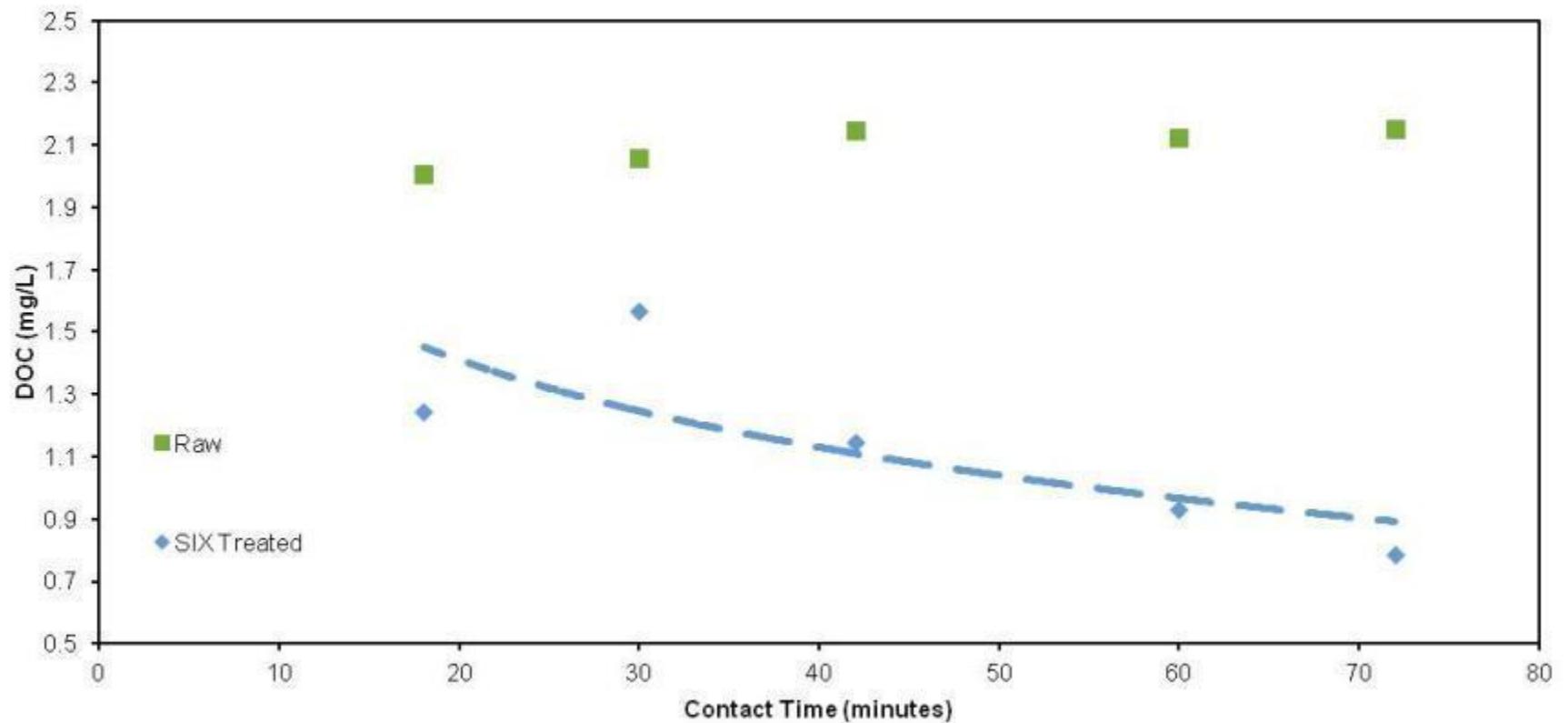


Process Flow Diagram for the SWW Pilot Study of SIX® and CeraMac®

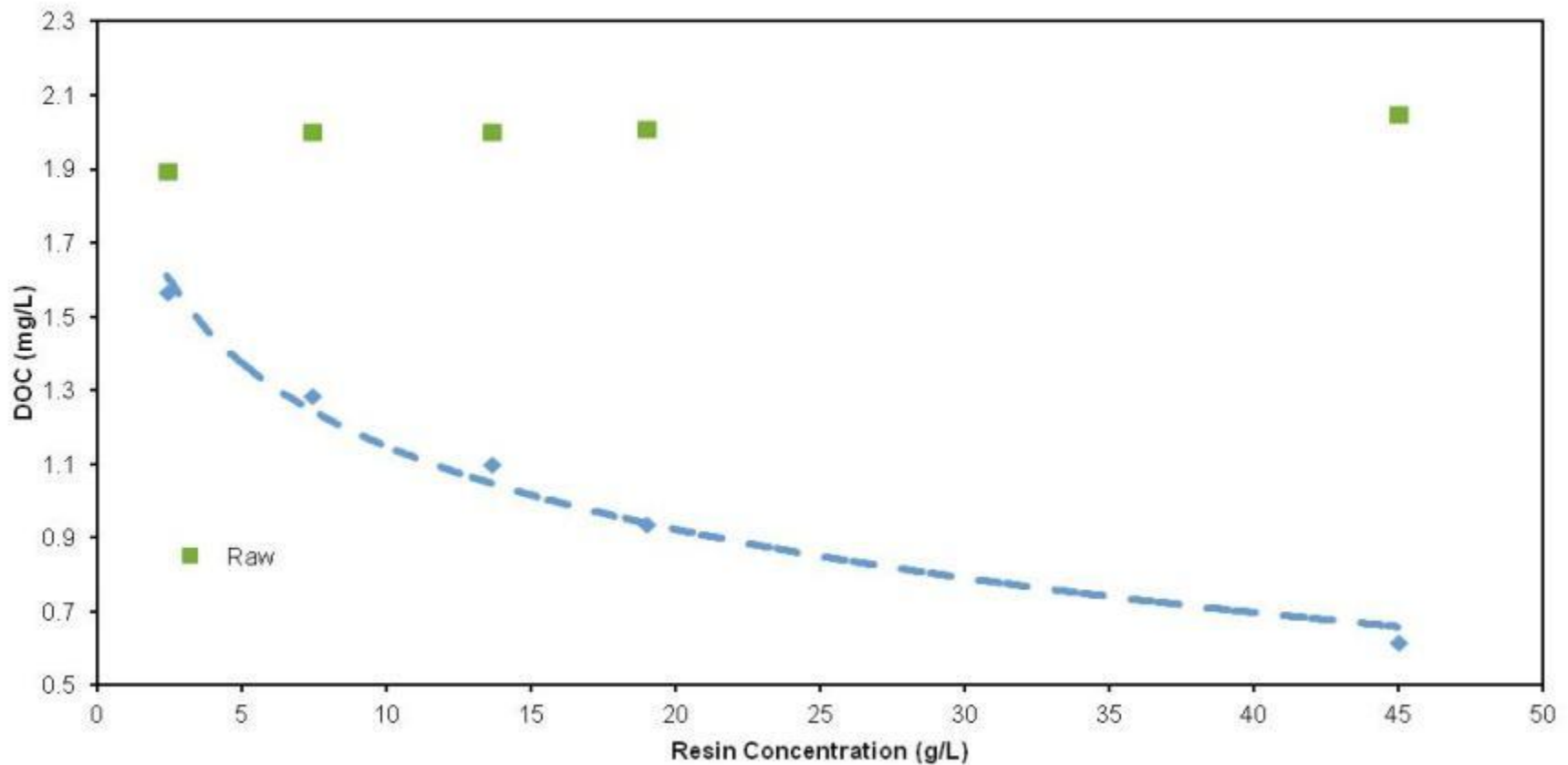
# Suspended ion exchange (SIX)

- Raw water flowing through 5 tanks in series
- A small dose of resin suspended in the raw water
- Good mixing (with air) and high turbulence
- Single pass (minimise risk of resin blinding)
- Goal is to minimise footprint/contact time and resin dose by keeping the kinetics fast
- Resin separation (lamella) and regeneration with multiple salt solutions

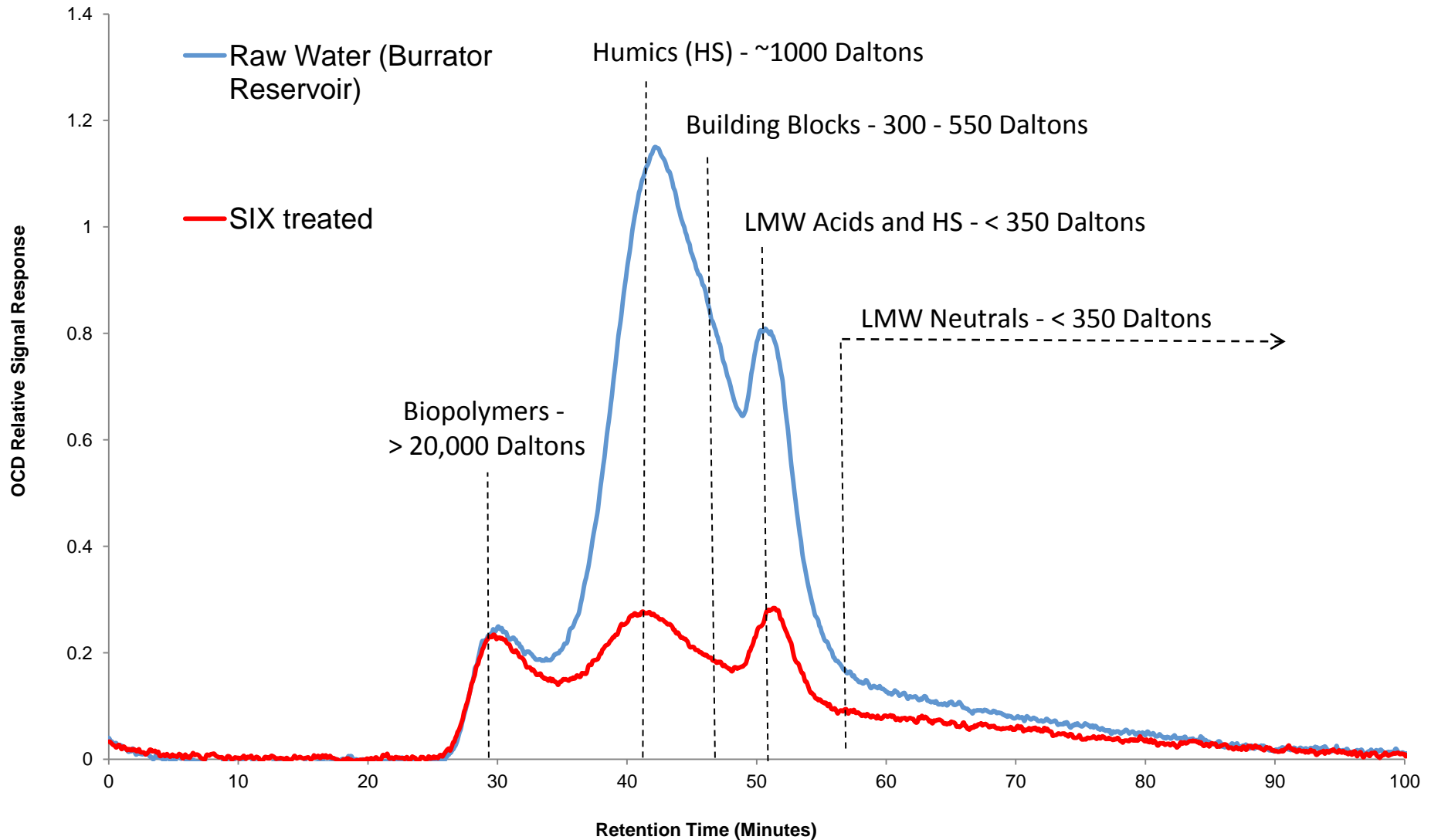
## SIX - Contact Time Matrix (10ml/l Resin)



## SIX - Resin Dose Matrix (30 Min Contact Time)



# Upland reservoir DOC removal by SIX (LC-OCD)

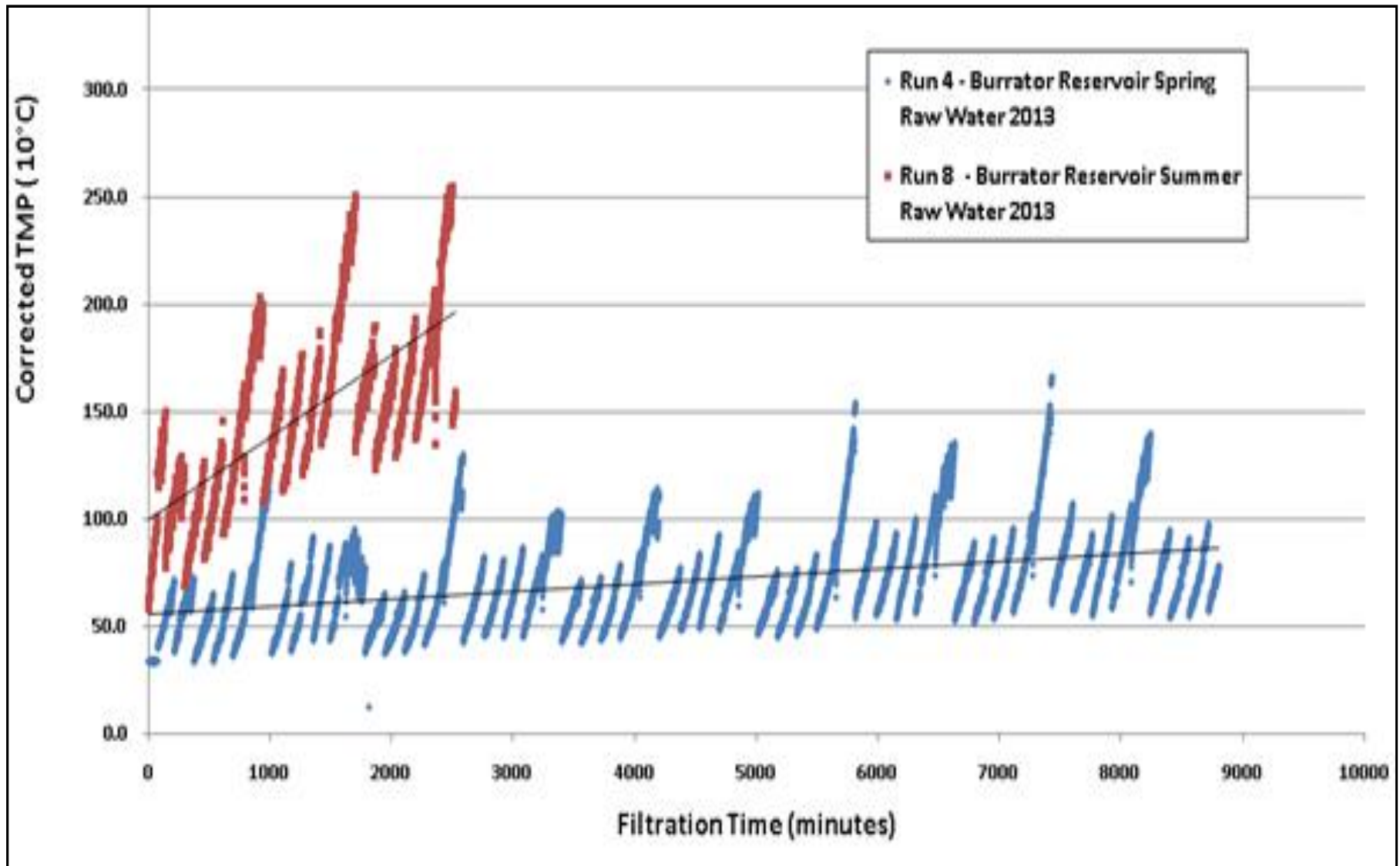


# Ceramic membranes

- Filtration area 25m<sup>2</sup> , 180mm x 1500mm
- Size of monolith cost effective
- Al<sub>2</sub>O<sub>3</sub> base layer TiO<sub>2</sub> top layer = 0.1um
- Close to 100 plants, no integrity failures
- High solids loading – direct river???
- Mechanical wash at high pressure
- Chemical cleaning options?
- Cost and recovery issues when applied traditionally

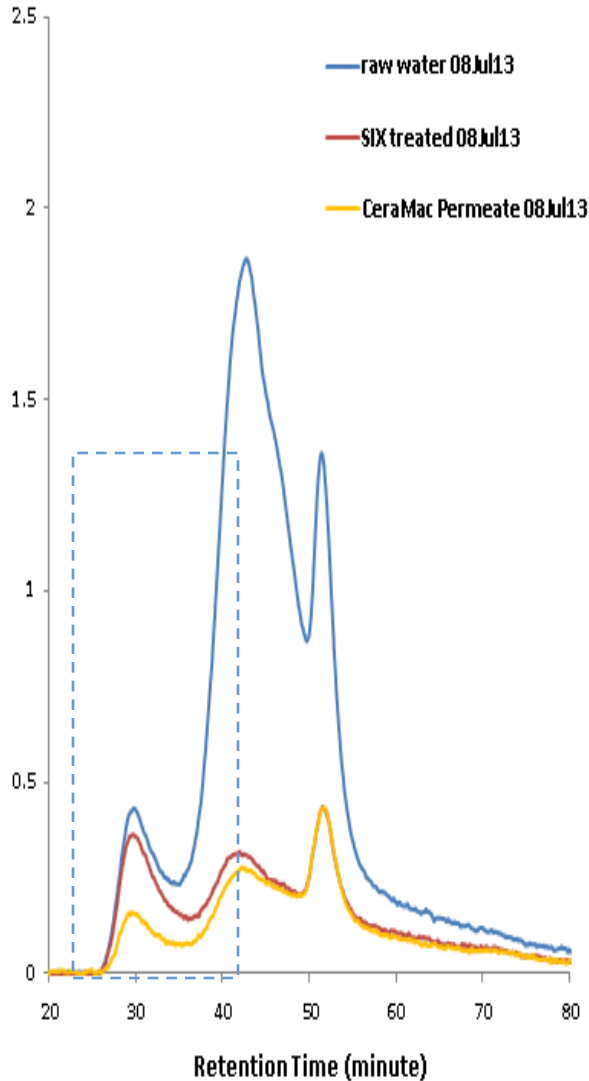


# Membrane testing and fouling

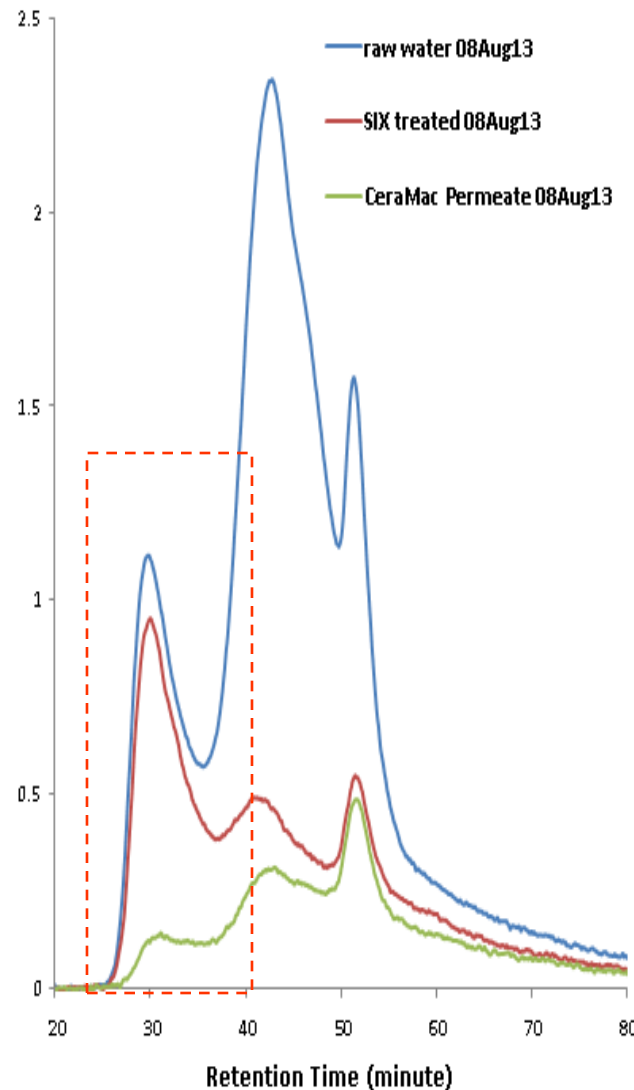


# Reservoir water quality change

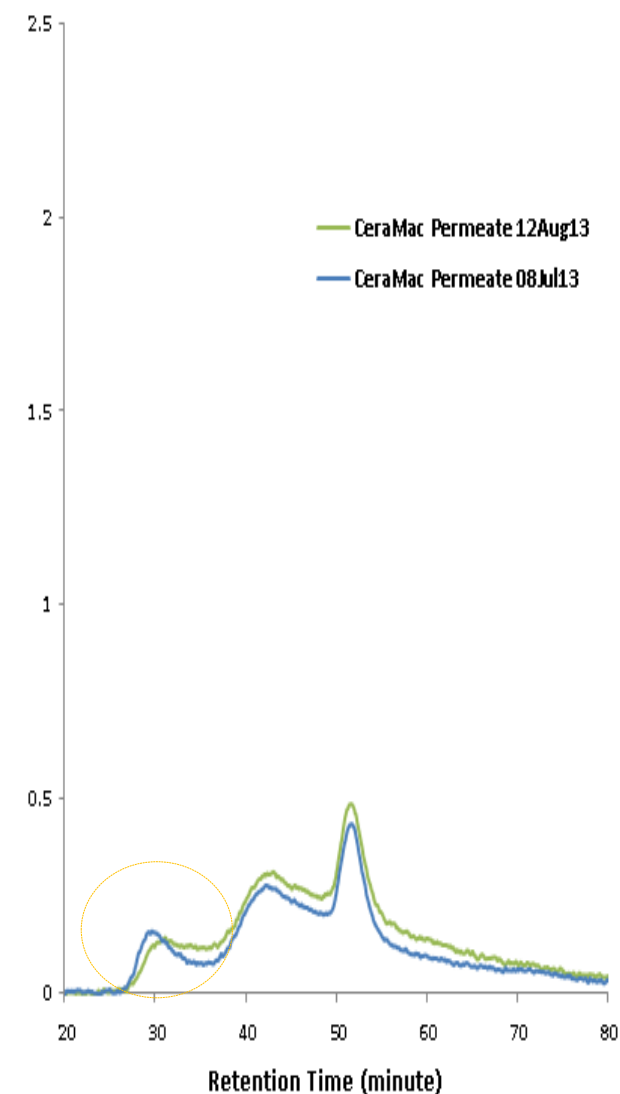
## Spring Quality



## Summer Quality

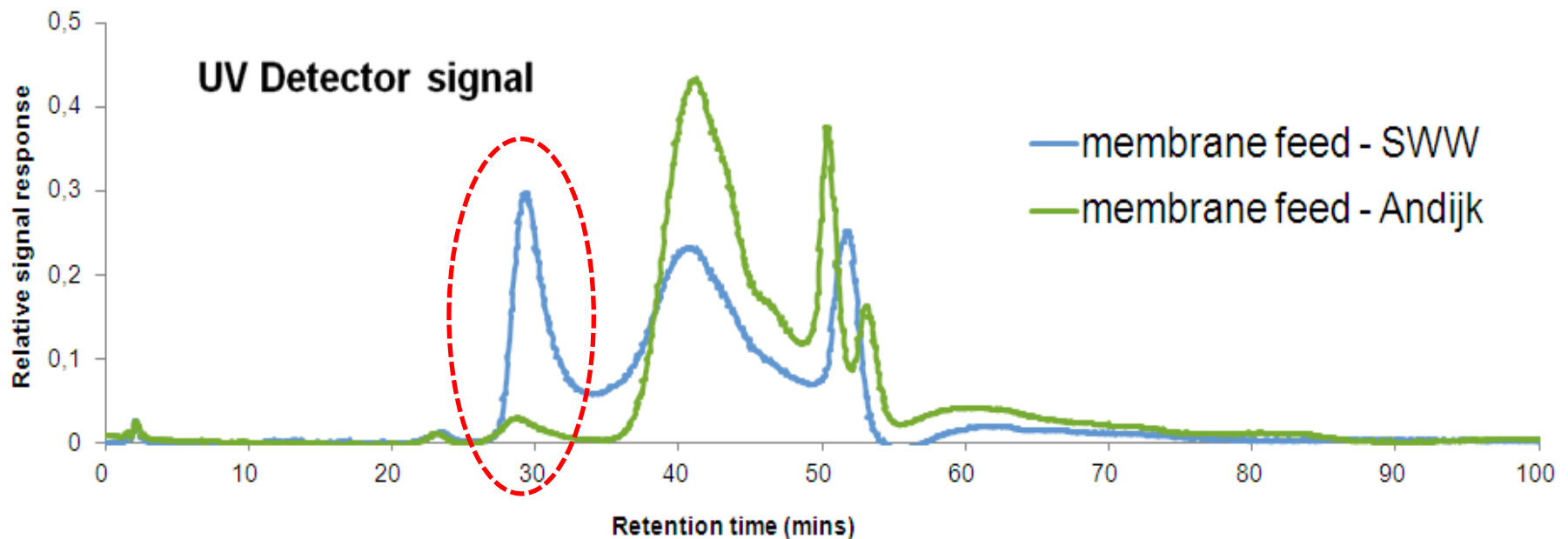
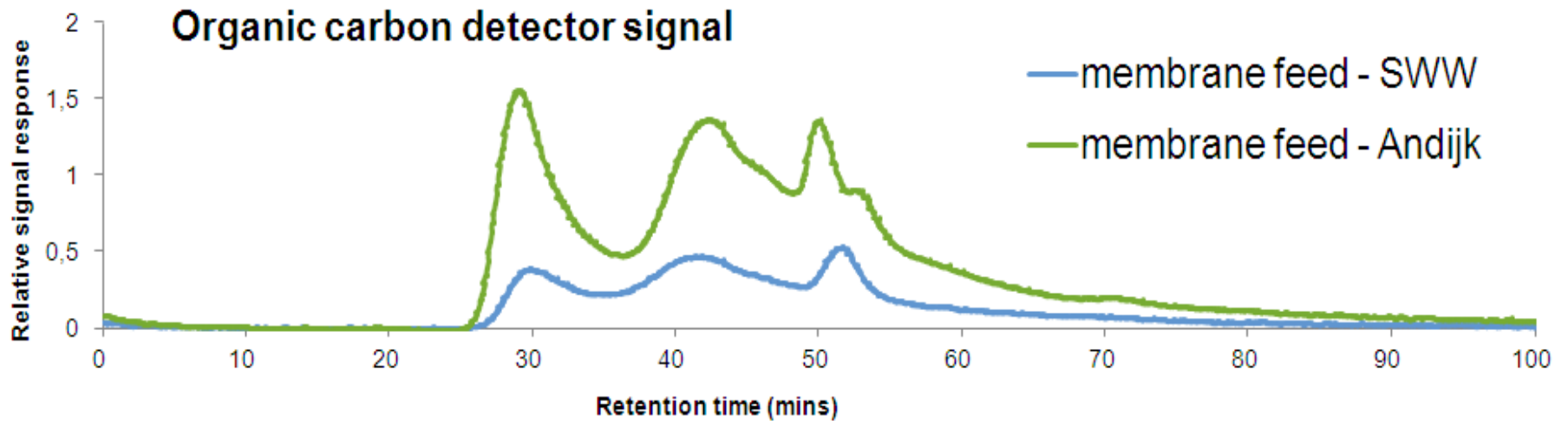


## Permeate Comparison

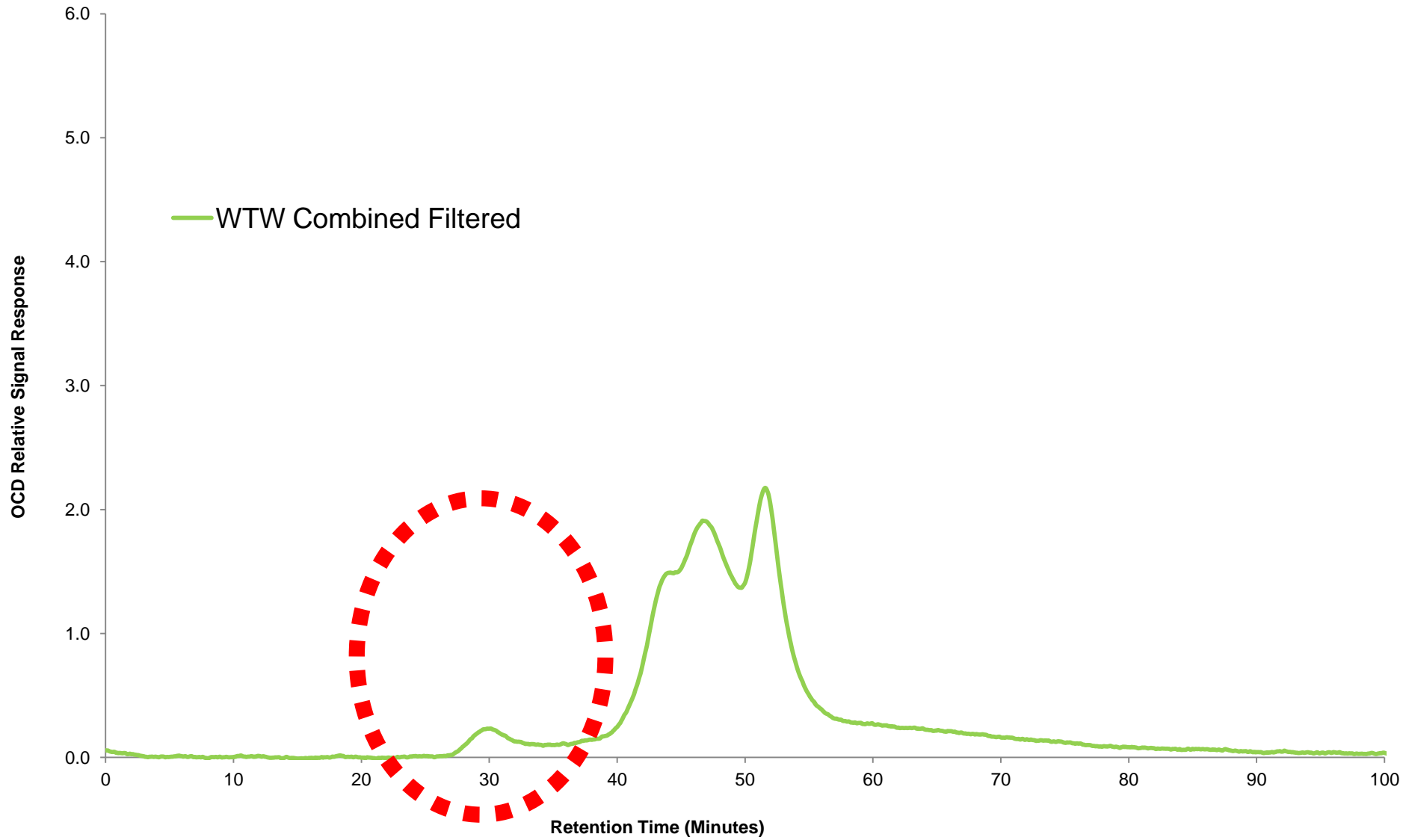




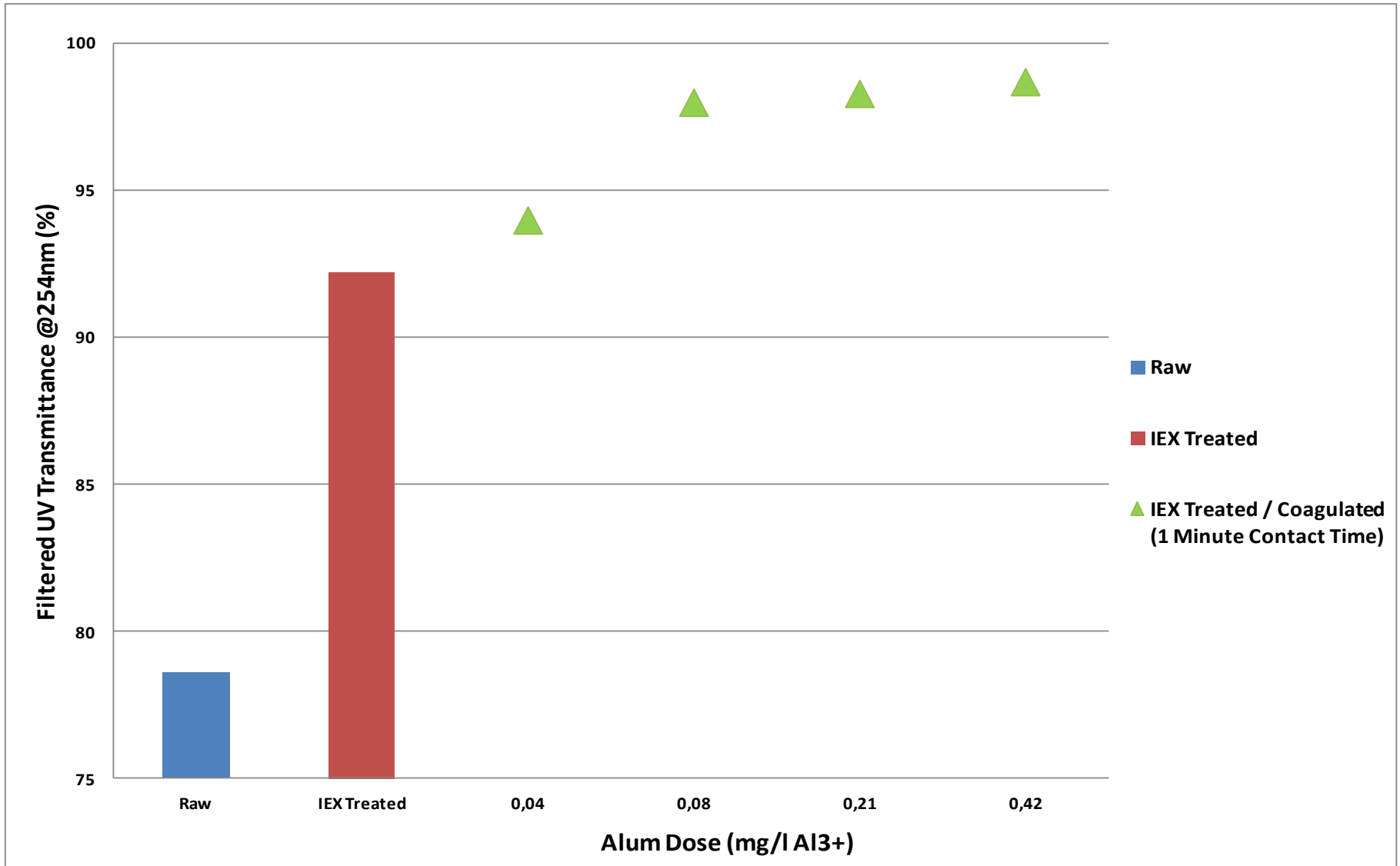
# DOC characteristics comparison



# Coagulation...

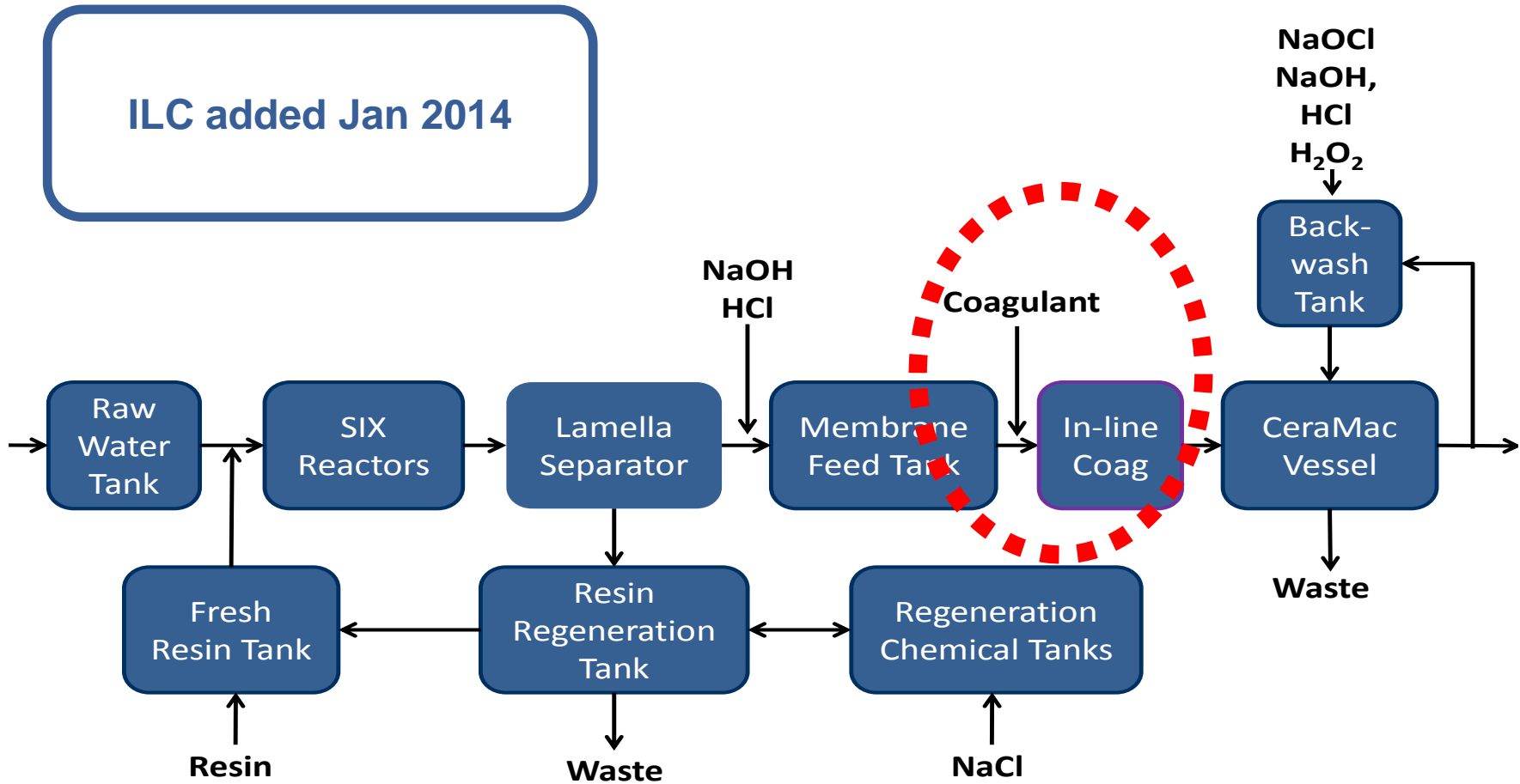


# Coagulant addition post SIX

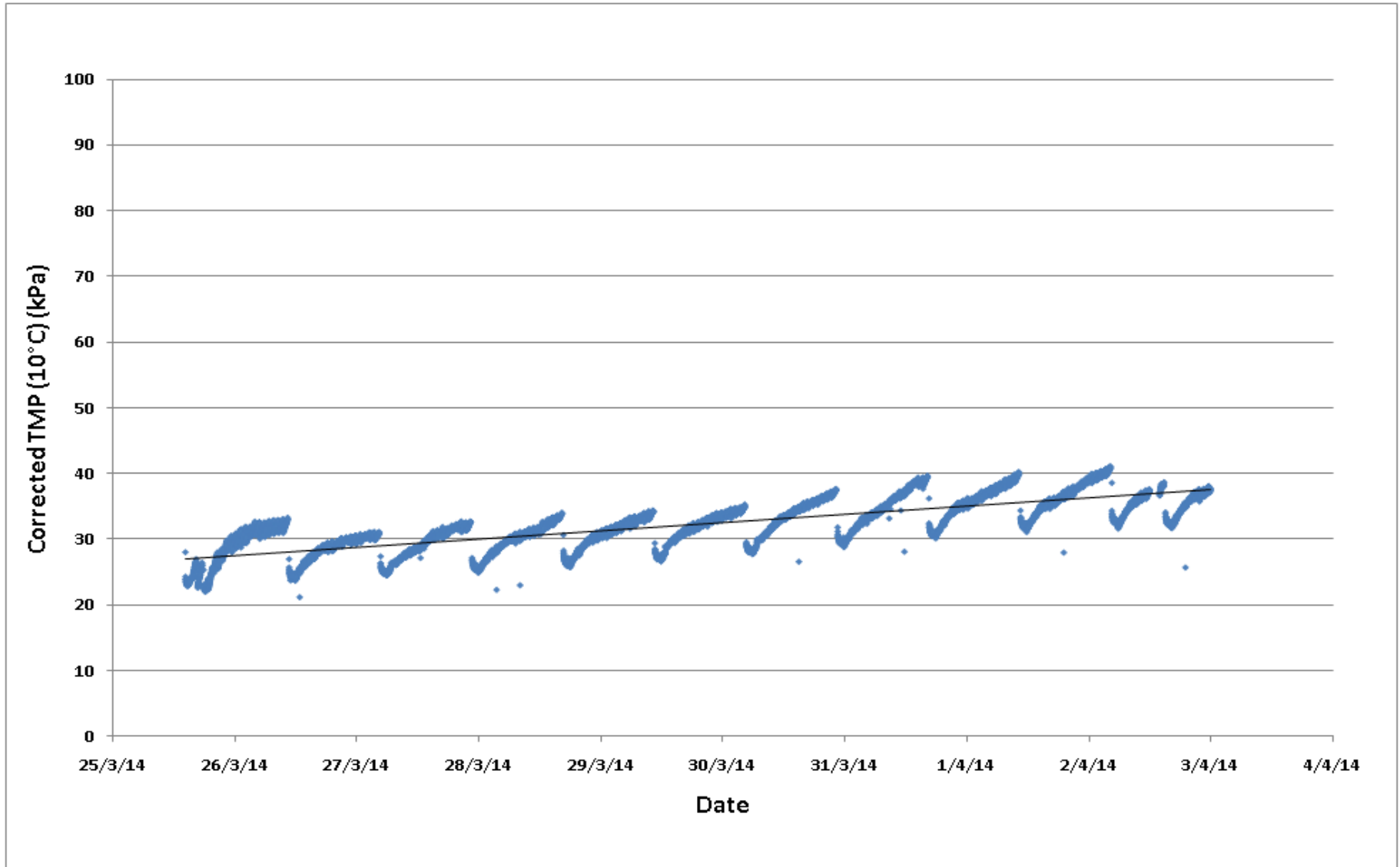


# Revised pilot process train

ILC added Jan 2014

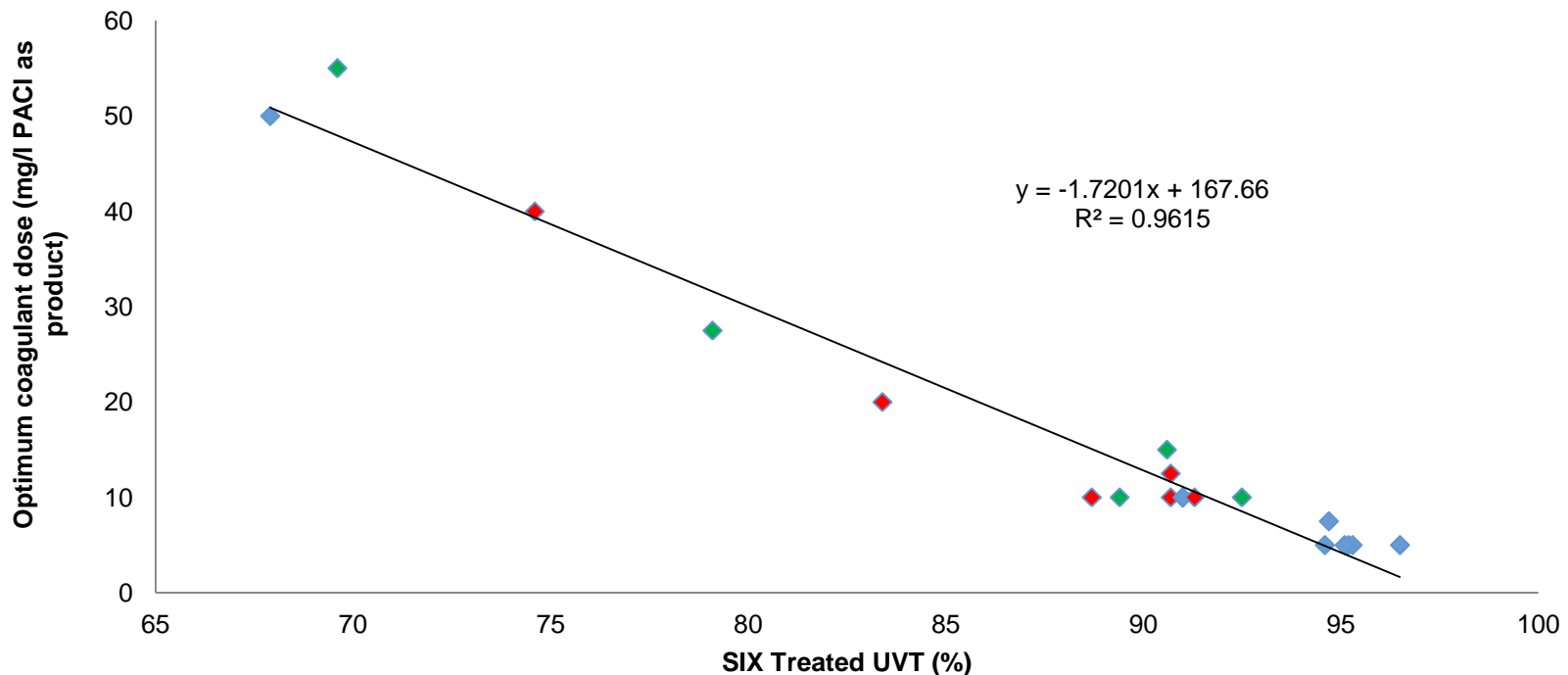


# SIX / ILCA pre-treatment

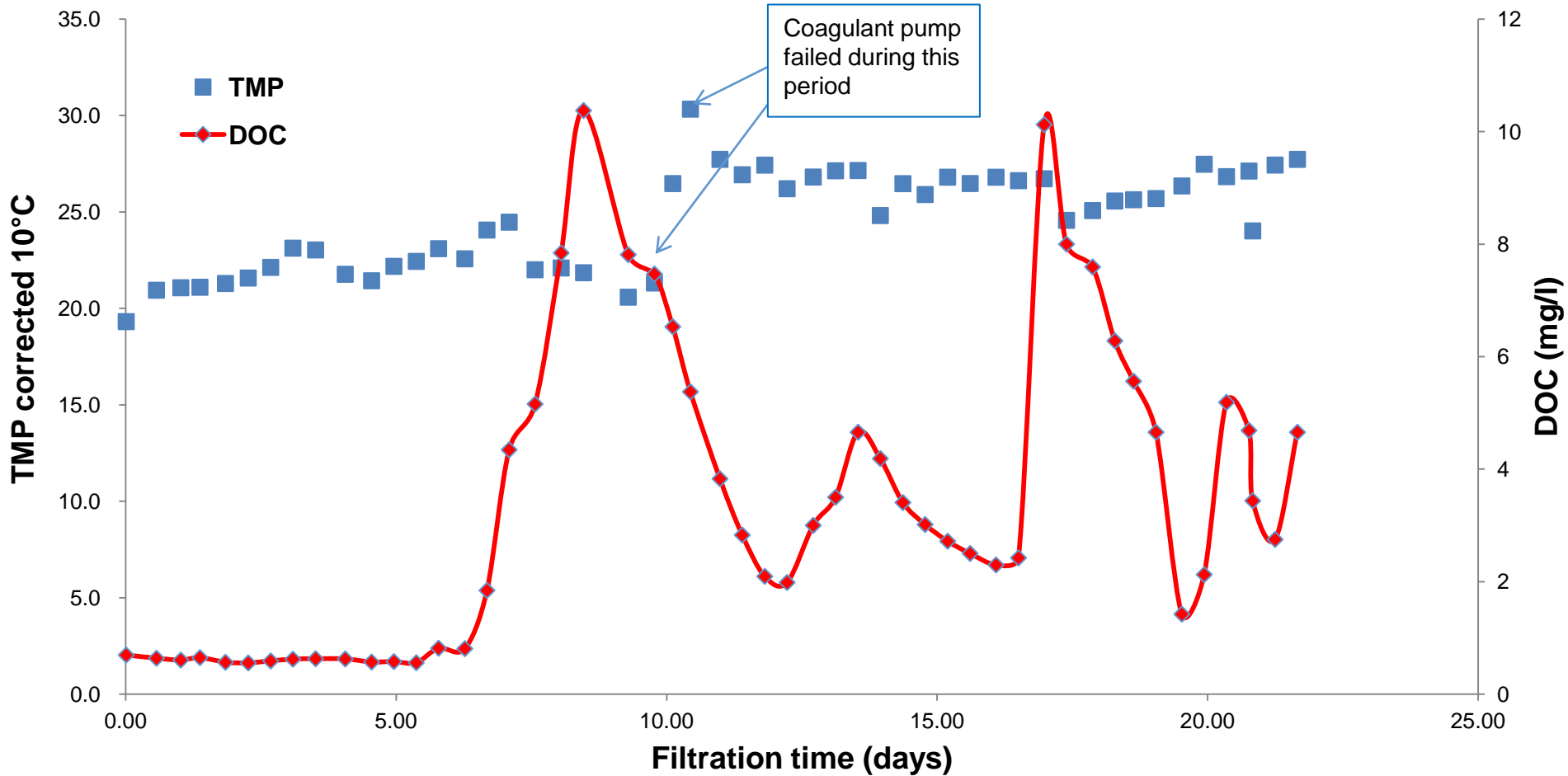


# Coagulant optimisation for MF

- New jar test method - less subjective + optimises organics removal
- 20 Jar tests on 3 sources + variable WQ
- Excellent correlation –  $r^2 = 0.96$



# Optimised membrane operation during spates

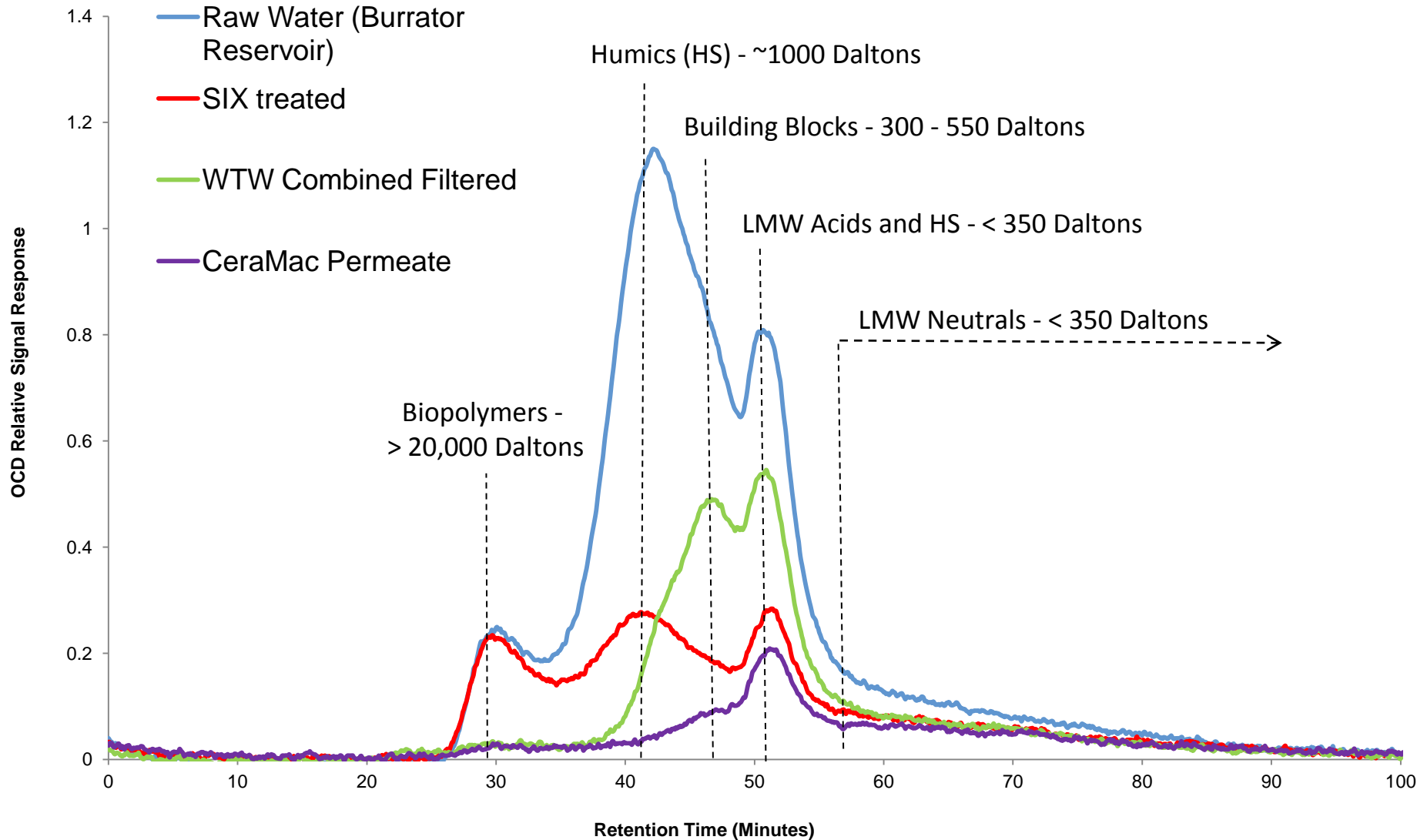


Optimised inline coagulation was critical to stable membrane operation. Using an automated coagulant control system it was possible to run at very high flux (185 LMH), during periods of extremely variable raw water quality (river spate conditions), with very low membrane fouling

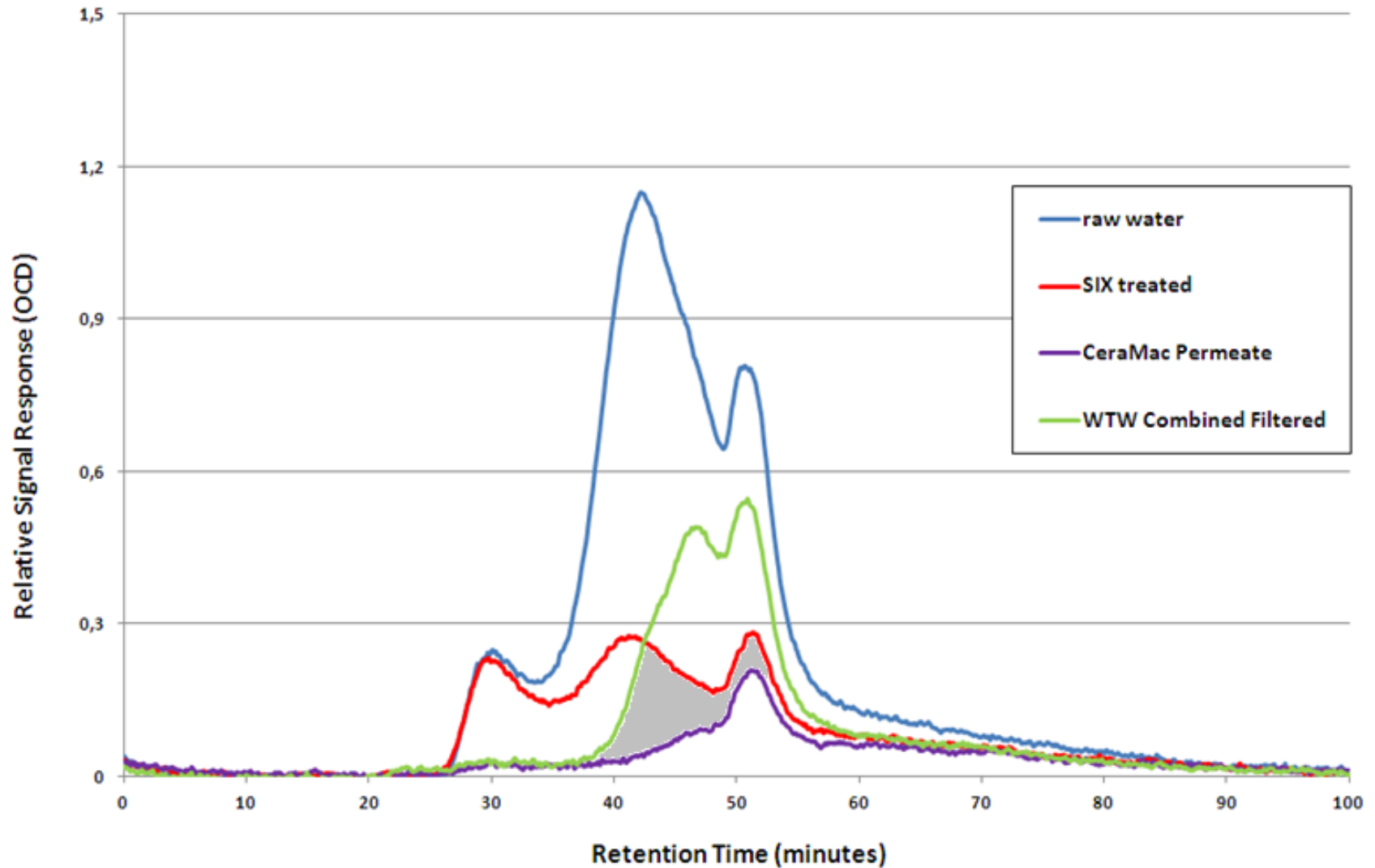
- Higher flux (SLR) = less membranes = lower cost
- Low fouling = simplifies operation, lowers pumping pressure, reduces frequency of chemical cleans
- A years worth of tests - All waters / conditions
- Sustainable flux determined as 185lmh max / 112lmh nominal – pilot info used for design
- Automation of coagulation and pH = improved performance



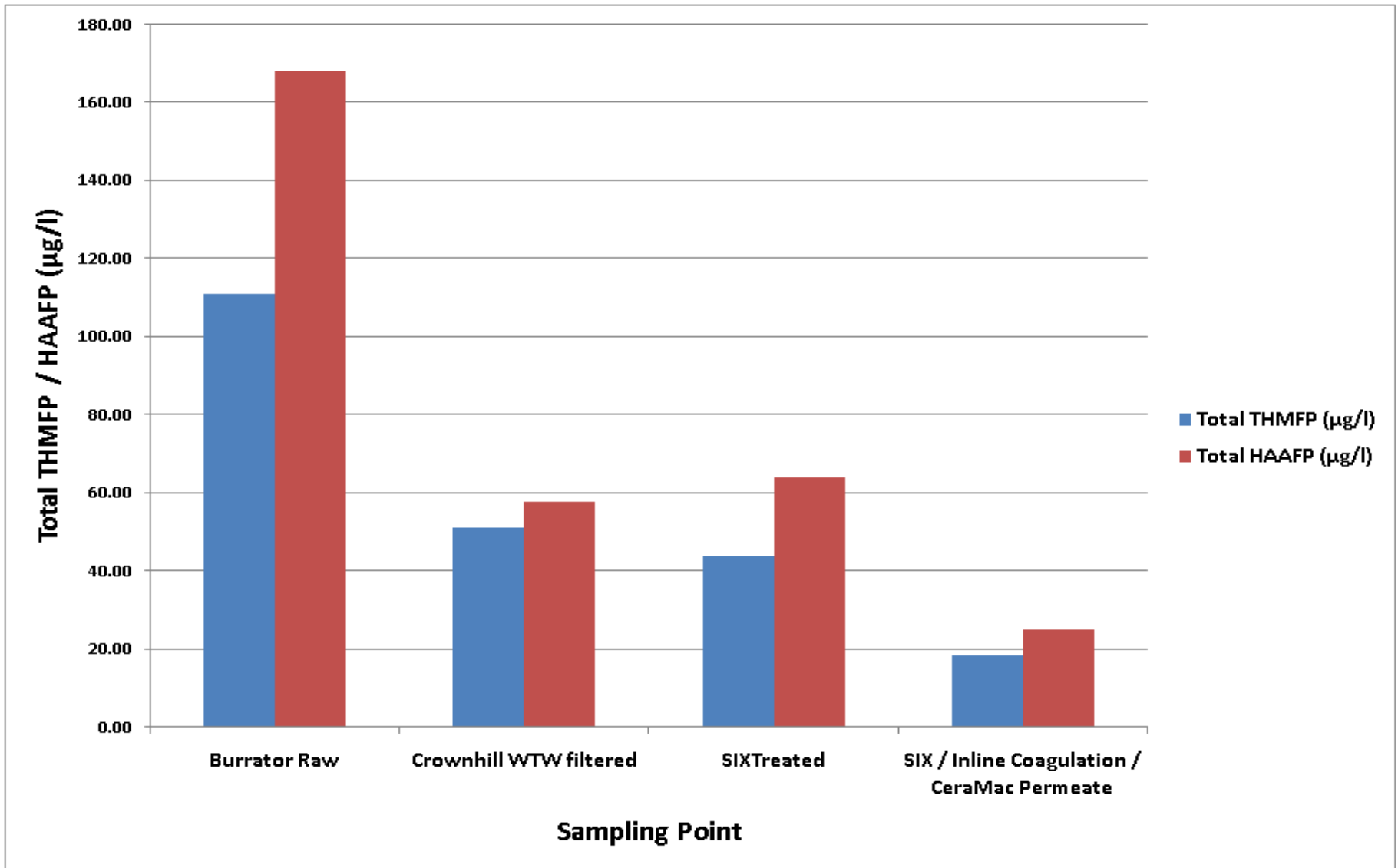
# Enhanced organics removal



# Organics removal



# By products



# Mean % removal SIX/ILCA vs. conventional

Parameter	SIX/ILCA/CeraMac additional removal relative to conventional treatment (%)
DOC (% Reduction)	50
UVA (% Reduction)	62
THMFP (% Reduction)	62
HAAFP (% Reduction)	62
THMFP Reactivity (% Reduction)	22
HAAFP Reactivity (% Reduction)	18
Brominated DBPFP (% Reduction)	47

- DBPFP reduction was not only due to enhanced DOC removal, but also to reduced concentrations of Br-DBPs and selective removal of reactive organic compounds

# Publications

CRANFIELD UNIVERSITY

David Christopher Metcalfe

Application of Suspended Ion Exchange, In-line Coagulation and Ceramic Membranes for Surface Water Treatment

School of Applied Science  
MSc by Research

Master of Science  
Academic Year: 2014 - 2016



Contents lists available at ScienceDirect

Water Research

journal homepage: [www.elsevier.com/locate/watres](http://www.elsevier.com/locate/watres)



## Removal of disinfection by-product precursors by coagulation and an innovative suspended ion exchange process



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<sup>c</sup> Department of Chemical Engineering, Qatar University, Qatar

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**Keywords:**  
Ceramic membrane filtration  
Disinfection by-products  
Ion exchange  
Natural organic matter

### ABSTRACT

This investigation aimed to compare the disinfection by-product formation potentials (DBFPs) of three UK surface waters (1 upland reservoir and 2 lowland rivers) with differing characteristics treated by (a) a full scale conventional process and (b) pilot scale processes using a novel suspended ion exchange (SIX) process and inline coagulation (ILCA) followed by ceramic membrane filtration (CMF). Liquid chromatography-organic carbon detection analysis highlighted clear differences between the organic fractions removed by coagulation and suspended ion exchange. Pretreatments which combined SIX and coagulation resulted in significant reductions in dissolved organic carbon (DOC), UV absorbance (UVA), trihalomethane and haloacetic acid formation potential (THMP, HAAFP), in comparison with the SIX or coagulation process alone. Further experiments showed that in addition to greater overall DOC removal, the processes also reduced the concentration of brominated DBPs and selectively removed organic compounds with high DBFP. The SIX/ILCA/CMF process resulted in additional removals of DOC, UVA, THMP, HAAFP and brominated DBPs of 50, 62, 62, 62% and 47% respectively compared with conventional treatment.



Contents lists available at ScienceDirect

Separation and Purification Technology

journal homepage: [www.elsevier.com/locate/seppur](http://www.elsevier.com/locate/seppur)



## Pre-treatment of surface waters for ceramic microfiltration



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<sup>c</sup> Qatar University, Doha, Qatar

### ARTICLE INFO

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Ceramic membrane  
Pre-treatment  
Ion exchange  
Coagulation  
Organic fouling

### ABSTRACT

The influence of pre-treatment on the suppression of irreversible (IR) fouling of ceramic membranes challenged with three UK surface waters has been studied at pilot scale. An initial scoping study compared the efficacy of suspended ion exchange (SIX) and clarification (coagulation followed by sludge blanket clarification) individually and in combination. Direct membrane filtration following in-line coagulation (ILCA) was also investigated with and without SIX. The impact on the various organic fractions, specifically high molecular weight (HMW) biopolymers (BPs) and humic substances (HS), and lower molecular weight (LMW) building blocks (BBs) and neutrals, was studied using liquid chromatography-organic carbon detection (LC-OCD).

Results revealed SIX and coagulation to preferentially remove the LMW and HMW organic fractions respectively. Residual HMW organic matter (primarily BPs) following SIX pre-treatment were retained by the membrane which led to rapid irreversible fouling. Coagulation pre-treatment provided stable membrane operation and the residual LMW organics were not significantly retained by the membrane. Combining clarification and SIX resulted in significantly increased removal of organics and lower fouling.



**NOTES**

- DO NOT SCALE FROM THE DRAWING. USE DIMENSIONS ONLY.
- ALL DIMENSIONS IN ALL LETTER UNLESS OTHERWISE.
- ALL LEVELS IN METERS RELATIVE TO ODN DATUM, MSL + 0.

**LEGEND**

**BUILDING STRUCTURES KEY:**

- RWA RAW WATER TANK
- SCB SOL AND CHAMIC BUILDING
- GAC GRANULAR ACTIVATED CARBON BUILDING
- CBT CHEMICAL BATCHING WATER TANK
- GEN GENERATOR BUILDING
- OFF OFFICE BUILDING
- TPS TURBINE PUMP STATION
- WPD WASTEWATER POWER DISTRIBUTION
- TWB TREATMENT WATER BASIN
- CSB CHEMICAL STORAGE BUILDING
- TUR TURBINE BUILDING
- TSR TREATMENT WATER RESERVOIR
- CBR CHEMICAL BATH BUILDING
- OFF OFFICE BUILDING
- UWU ULTRA-Ultraviolet TREATMENT BUILDING
- SCR SCREENING BUILDING
- LAM LABEL BUILDING

**KEY:**

- Red line: SITE BOUNDARY
- Black line with arrows: PROPOSED ENHANCED BOUNDARY

**REVISIONS:**

NO	UPDATED	
NO	UPDATED	
NO	FOR INFORMATION	

**Task:** PRELIMINARY  
NOT TO BE USED FOR CONSTRUCTION

Scale:	1:500	Client Scale:	1:1000
Original Size:	A1	Checker:	C. Jones
Drawn:	NEWLYN	Drawn:	M. Jones
Rev:	05	Rev:	01

**Project:** SOUTH WEST WATER K6 PROGRAMME NORTH PLYMOUTH

**Site:** NORTH PLYMOUTH W PROPOSED SITE LAYOUT

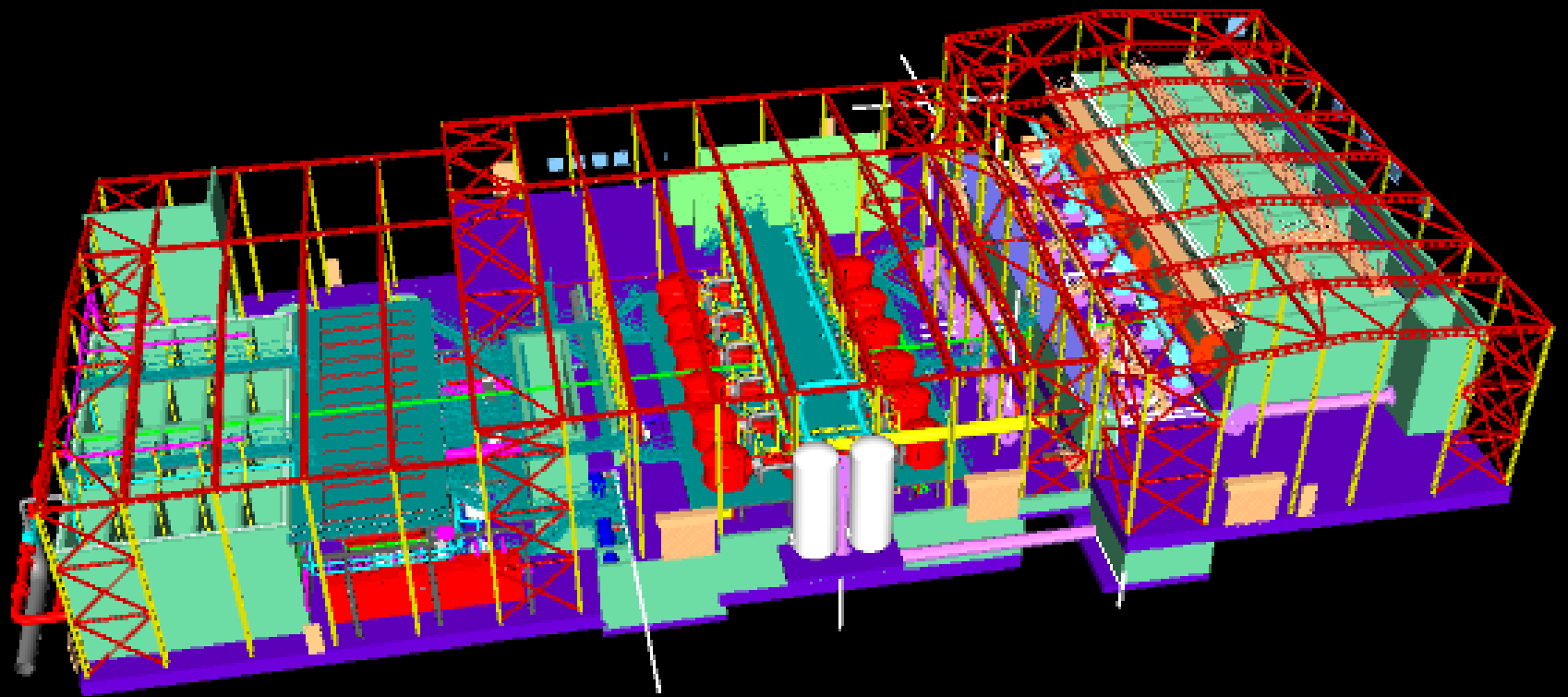
**Document Reference:** NPLY-ARC-ROW-XX-DR-C-10120

**Drawn Project Number:** 30006373

**Scale:** 1:500

**Scale Bar:** 0 10 20 30 40 50m

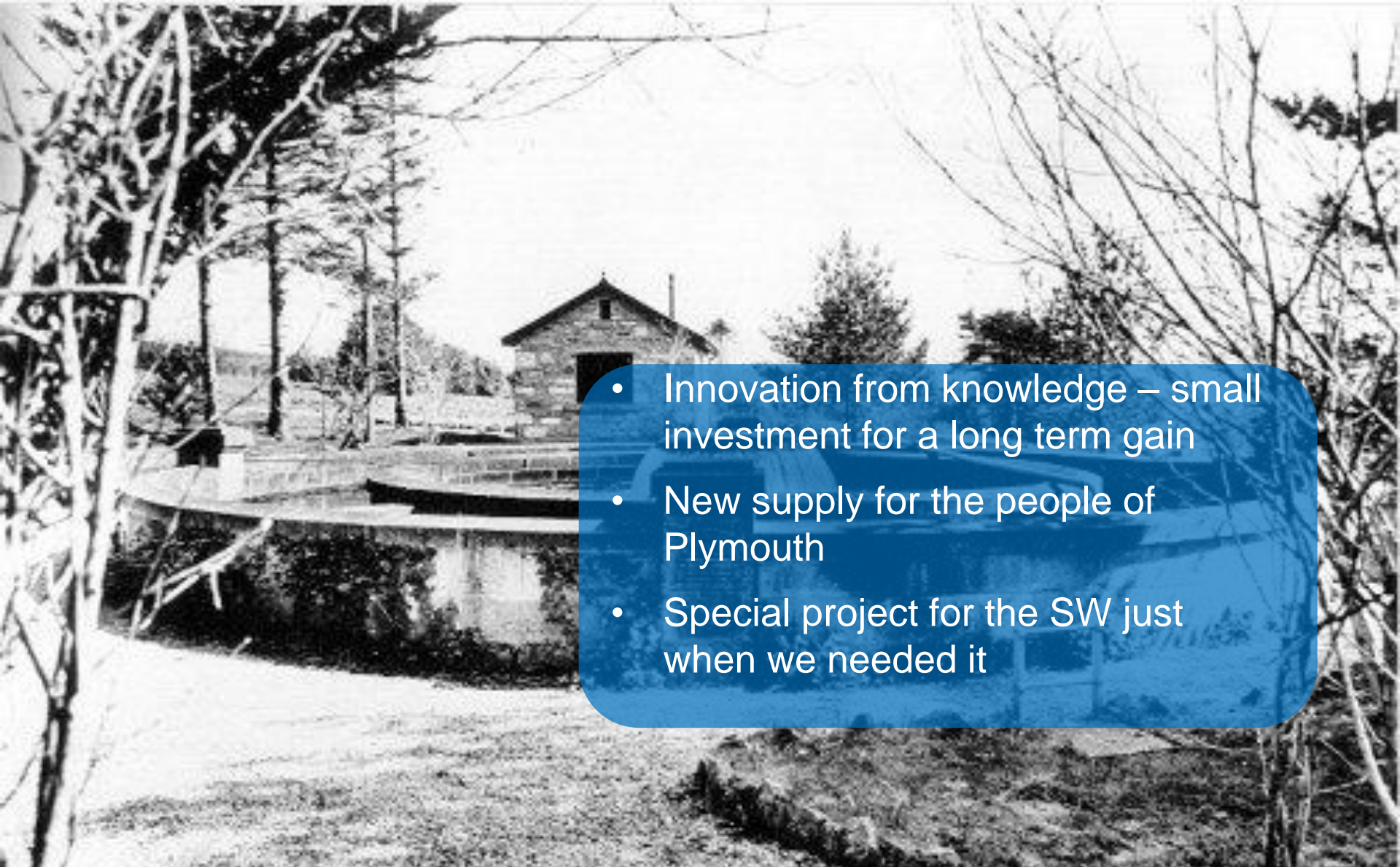
**Watermark:** DRAFT FOR CONSULTATION ONLY







# Summary

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- Innovation from knowledge – small investment for a long term gain
  - New supply for the people of Plymouth
  - Special project for the SW just when we needed it

# Acknowledgments...



*Cranfield*  
UNIVERSITY

**Rwb** waterservices

DOC2C'S

HET  WATERLABORATORIUM

Thank you



When trying to protect your membranes...

‘...dubbel genaaid houdt beter!’