# Ceramic microfiltration; a novel and compact process for the treatment of surface water

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### Acknowledgement





### Contents



- Motive and opportunity
- In-line coagulation, ceramic microfiltration
- DOC, membrane fouling and DBPs
- Full scale application/footprint

#### Who we serve...











### **Opportunity**













#### Reviewed and re-stated treatment goals

- Absolute Barrier to Cryptosporidium
- DOC / disinfection by product reductions
- <u>Very compact</u>, forward looking design
- Highly automatable, robust and efficient process
- Environmental impact/sustainability
- Keep consumer bills down in long term

### **Ceramic membranes**



- Filtration area 25m<sup>2</sup>, 180mm x 1500mm
- Size of monolith cost effective
- $AI_2O_3$  base layer  $TiO_2$  top layer = 0.1um
- Close to 100 plants, no integrity failures
- High solids loading direct river???
- Mechanical wash at high pressure
- Chemical cleaning options?
- Cost and recovery issues when applied traditionally







## **Critical flux testing**



- a) 150 lmh low algal loading
- a) 200 lmh low algal loading
- a) 200 lmh high algal loading
- a) 250 lmh high algal loading





### Membrane fouling / sustainable flux

Higher flux (SLR) = less membranes = lower cost Low fouling = simplifies operation, lowers pumping pressure, reduces frequency of chemical cleans Sustainable flux determined as c185/136lmh

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### Alternative CIP approach





# LC-OCD organic removal comparison outh WEST WATER



OCD relative signal response



### By products



### Footprint reduction and buildability





### Optimised membrane operation during spates



Optimised inline coagulation was critical to stable membrane operation. Using an automated coagulant control system it was possible to run at very high flux (185 LMH), during periods of extremely variable raw water quality (river spate conditions), with very low membrane fouling

### Mean % removal SIX/ILCA vs. conventional

Parameter	SIX/ILCA/CeraMac additional removal relative to conventional treatment (%)
DOC (% Reduction)	50
UVA (% Reduction)	62
THMFP (% Reduction)	62
HAAFP (% Reduction)	62
THMFP Reactivity (% Reduction)	22
HAAFP Reactivity (% Reduction)	18
Brominated DBPFP (% Reduction)	47

• DBPFP reduction was not only due to enhanced DOC removal, but also to reduced concentrations of Br-DBPs and selective removal of reactive organic compounds

## **Publications**





Received in revised form 35 February 2016

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Repairing

Pretrating ment

ton exchange

Organier fooling

Coagulation

Ceratilic membrane

Available online 26 February 2016

Master of Science Academic Year: 2014 - 2016 lenged with three UK surface waters has been studied as pilot scale. An initial scoping study compared the efficacy of suspended ion exchange (SIX) and clarification (couplation followed by shadge blanker clarification) individually and in combination. Direct membrane filtration following in-line couplation (BCA) was also investigated with and without SIX. The inspact on the various organic fractions, specifically high molecular weight (HMV) biopolymers (IPF) and hume substances (HSA), and lower molecular weight (LMW) building blocks (BBs) and neutrals, was studied using liquid chromatography-organic carbon detection (IC-OCD). Results neveraled SIX and couplation to preferentially remove the LMW and HMW organic fractions.

Results revealed SIX and cognitation to preferentially remove the LMW and HMW neganic fractions respectively. Residual HMW organic matter (primarily IIPs) following SIX pre-treatment were related by the membrane which led to rapid increversible fouling. Cognitation pre-treatment provided stabile membrane operation and the residual LMW organics were not significantly retained by the membrane.





- Innovation from knowledge small investment for a long term gain
- New supplies for the people of Falmouth and Plymouth
- Special projects for the SW just when we needed it

### Acknowledgments...





### Thank you



# Good, safe, drinking water that has the trust of our consumers